

Alternative implementation of a porous media model for simulating drying of heated concrete

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Motivation



Photo CSTB

- When exposed to high temperatures (fire), concrete can spall.
- Spalling: violent detachment of flakes
- Severe damage in tunnels after fire
- Presumable causes:
 - Pore pressure increase due to evaporation and dehydration
 - Thermal stresses

Introduction (1)

- Porous medium, partially saturated
 - Gas (air+vapor) and liquid phase
 - Heat and moisture transfer
 - Vapor sources: evaporation and dehydration
 - Mechanical stresses not considered

 - Single classical formulation for concrete in literature (presented in previous COMSOL conference)
 - Uses capillary pressure as primary variable
 - Vapor pressure from phase equilibrium
- } undefined for $S=0$
and for $T > T_{cr}$ (374°C)

Introduction (2)

- Different implementations for other applications
 - Food drying
 - Oil and gas exploration
 - Compressible / incompressible phases
 - With or without phase change
- Alternative formulation
 - Non-equilibrium: evaporation rate from deviation of vapor pressure from equilibrium pressure
- Use weak form interface

Conservation equations

$$\frac{\partial}{\partial t} \text{density} + \nabla \cdot \text{flux} + \text{convec} \cdot \nabla u = \text{source}$$

- Gas conservation $\rho_g = \rho_a + \rho_v$

$$\frac{\partial}{\partial t} (\phi(1-S)\rho_g) + \nabla \cdot (\rho_g \mathbf{v}_g) = \dot{m}_{\text{evap}} + \dot{m}_{\text{dehyd}}$$

- Vapor mass fraction $\omega_v = \rho_v / \rho_g$

$$\phi(1-S)\rho_g \frac{\partial \omega_v}{\partial t} + \nabla \cdot \mathbf{j}_v + \underbrace{\rho_g \mathbf{v}_g}_{\text{convection}} \cdot \nabla \omega_v = (1-\omega_v)(\dot{m}_{\text{dehyd}} + \dot{m}_{\text{evap}})$$

- Liquid conservation

$$\frac{\partial}{\partial t} (\phi S \rho_l) + \nabla \cdot (\rho_l \mathbf{v}_l) = -\dot{m}_{\text{evap}}$$

- Energy conservation

$$\rho c_p \frac{\partial T}{\partial t} + \nabla \cdot (\underbrace{-k_{\text{eff}} \nabla T}_{\text{heat conduction}}) + \underbrace{(\rho_v c_{pv} \mathbf{v}_v + \rho_a c_{pa} \mathbf{v}_a)}_{\text{convection}} \cdot \nabla T = -\dot{m}_{\text{dehyd}} \Delta h_{\text{dehyd}} - \dot{m}_{\text{evap}} \Delta h_{\text{evap}}$$

Dependent variables and BC

- Dependent variables
- Conservative Flux
- Dirichlet BC → dependent variable
Neumann BC → conservative flux

$$p_g$$

$$\rho_g \mathbf{v}_g$$

$$p_g = p_g^{amb}$$

$$\omega_v = \rho_v / \rho_g$$

$$\mathbf{j}_v = -\rho_g D_{eff} \nabla \omega_v$$

$$-\mathbf{n} \cdot \mathbf{j}_v = 0 \quad \text{constant mixture}$$

$$S$$

$$\rho_l \mathbf{v}_l$$

$$-\mathbf{n} \cdot (\rho_l \mathbf{v}_l) = -K_0^l \langle p_l - p_g^{amb} \rangle^+ \quad \text{outflow}$$

$$T$$

$$-k_{eff} \nabla T$$

$$-\mathbf{n} \cdot (-k_{eff} \nabla T) = h_T (T_{ext} - T) + \varepsilon \sigma (T_{ext}^4 - T^4)$$

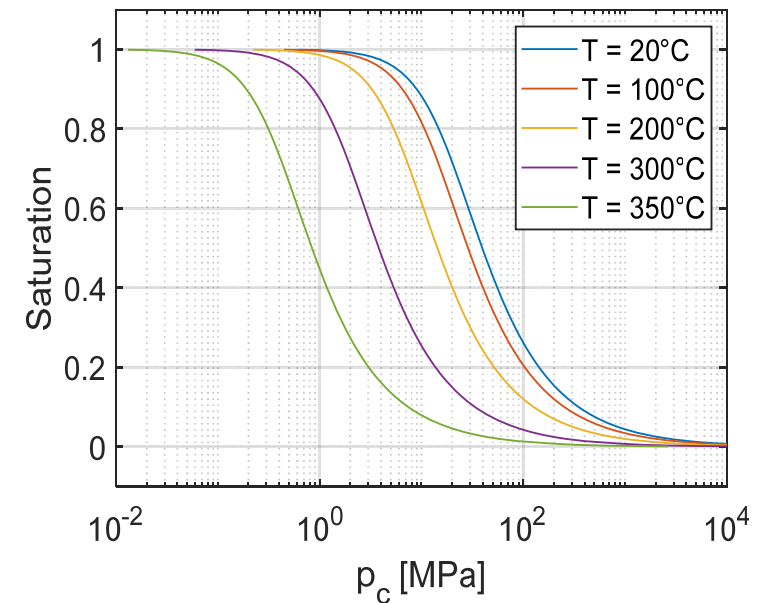
- Choice of primary variables and equations influences formulation of BCs

Capillary effects

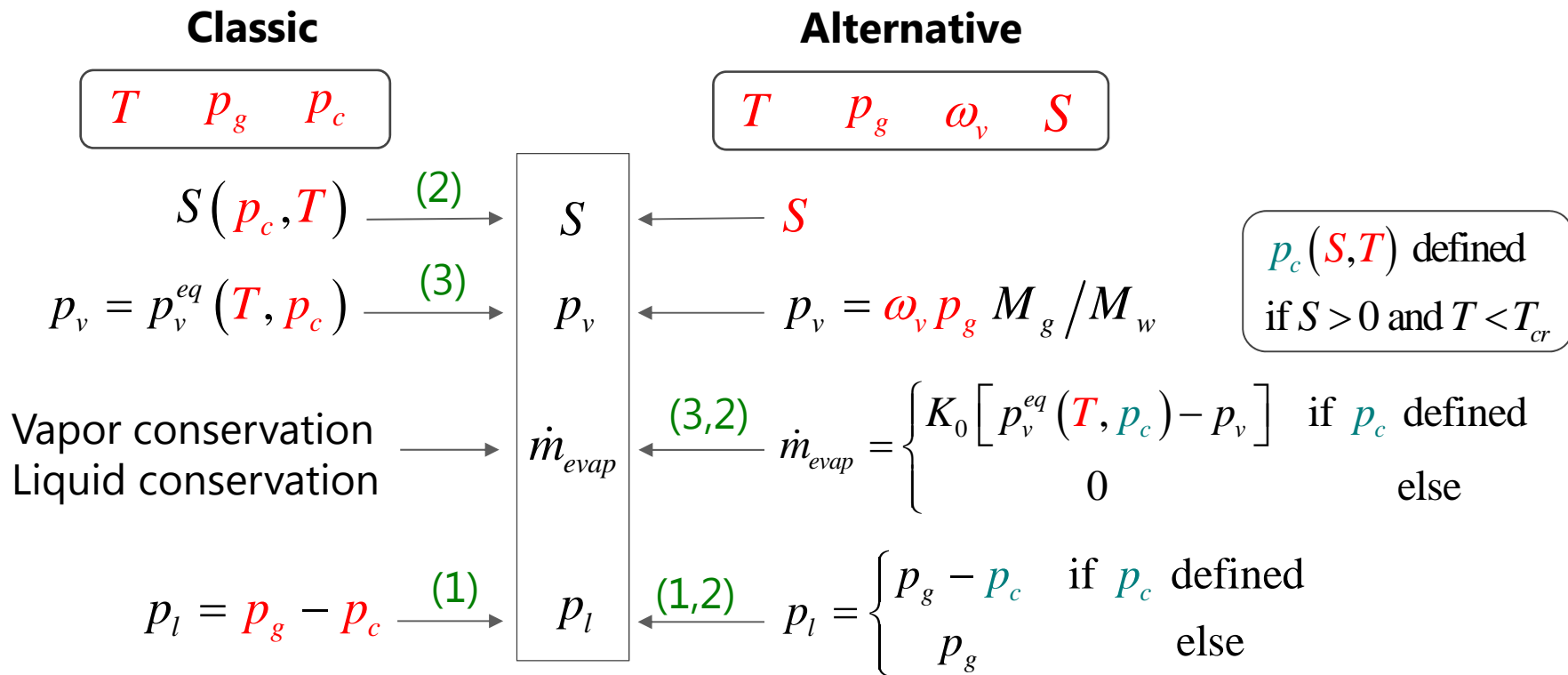
- (1) Capillary pressure $p_c = p_g - p_l$
- (2) Sorption isotherms (van Genuchten)
→ Description of porous medium

$$S = \left[1 + \left(\frac{p_c^{amb}}{a} \right)^{\frac{b}{b-1}} \right]^{-1/b} \quad p_c = p_c^{amb} \left(\frac{T_{cr} - T}{T_{cr} - T_{amb}} \right)^N$$

- (3) Vapor saturation pressure (Kelvin)
$$p_v^{eq} = p_{sat}(T) \cdot \exp\left(\frac{-p_c M_w}{\rho_l RT}\right)$$



Connecting variables with capillary effects

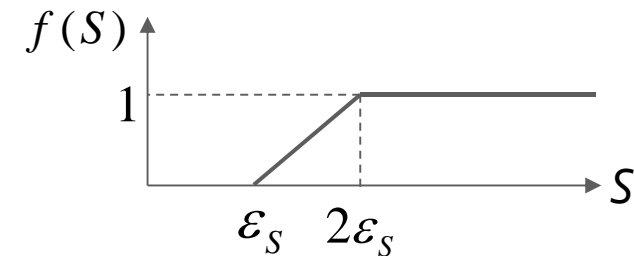


(1) Capillary pressure (2) Sorption isotherm (3) Vapor saturation pressure

Regularization (1)

- Stop evaporation if $S=0$ or $T > T_{cr}$
- Only evaporation restricted, not condensation

$$\Delta p_v = \underbrace{\langle p_v^{eq} - p_v \rangle^+}_{\text{positive part evaporation}} \underbrace{\frac{\max(S - \varepsilon_S, 0)}{\max(S - \varepsilon_S, \varepsilon_S)}}_{f(S)} + \underbrace{\langle p_v^{eq} - p_v \rangle^-}_{\text{negative part condensation}}$$



- Also restriction with temperature

$$\dot{m}_{evap} = K_0^{evap} \frac{M_w}{RT} \Delta p_v \frac{\max(T - T_{cr} - \varepsilon_T, 0)}{\max(T - T_{cr} - \varepsilon_T, \varepsilon_T)}$$

Regularization (2)

- van Genuchten not invertible for $S=0$

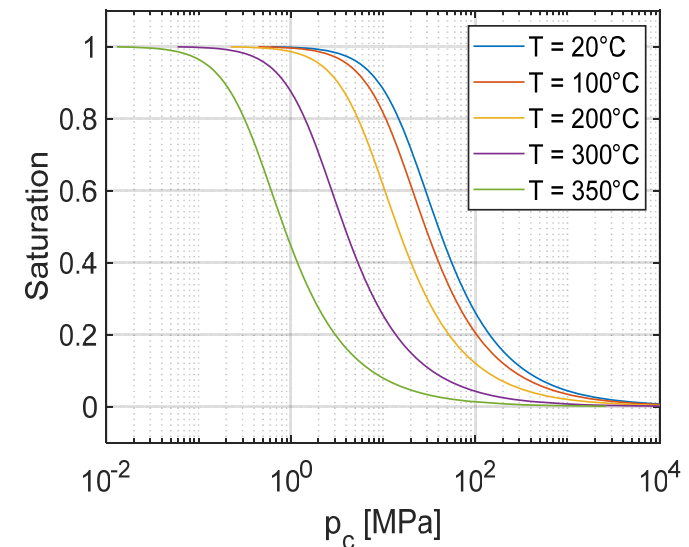
$$p_c^{amb} = a(S^{-b} - 1)^{(1-1/b)}$$

- Relative liquid permeability also undefined for $S=0$

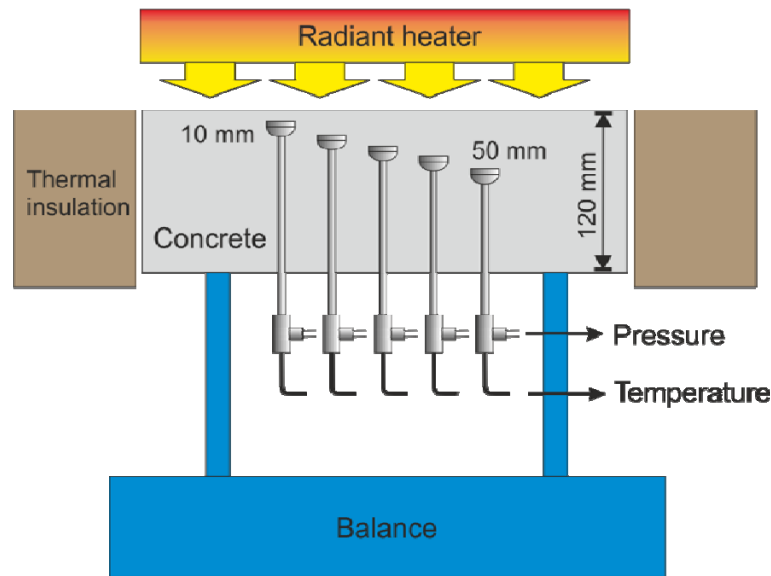
$$\kappa_{rl} = \sqrt{S} \left[1 - (1 - S^b)^{1/b} \right]^2$$

- For relative permeability and saturation use

$$S_{reg} = \max(S, \varepsilon_s)$$



Experiment

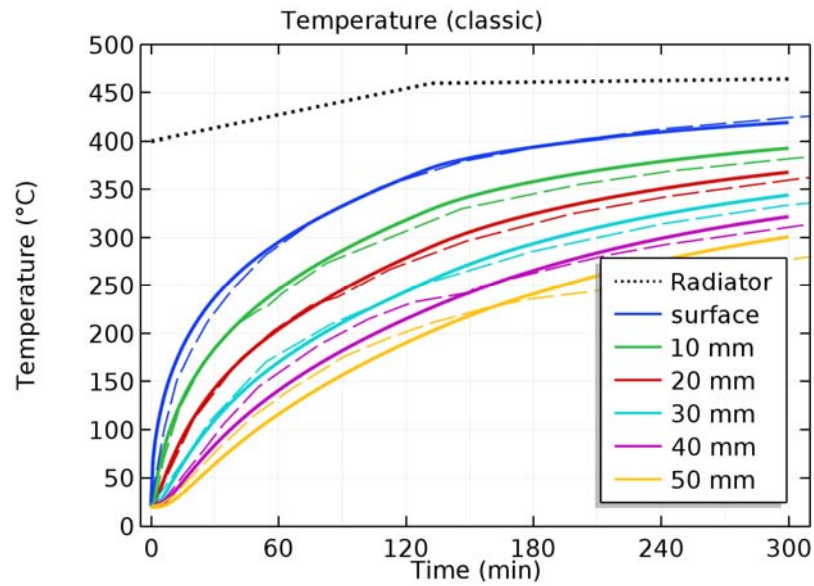


- 12-cm-thick concrete slab 30 x 30 cm²
- Pressure and temperature sensors
- Heated with radiator from top during several hours
- Not all material parameters are provided in the paper: others from literature or by calibration.

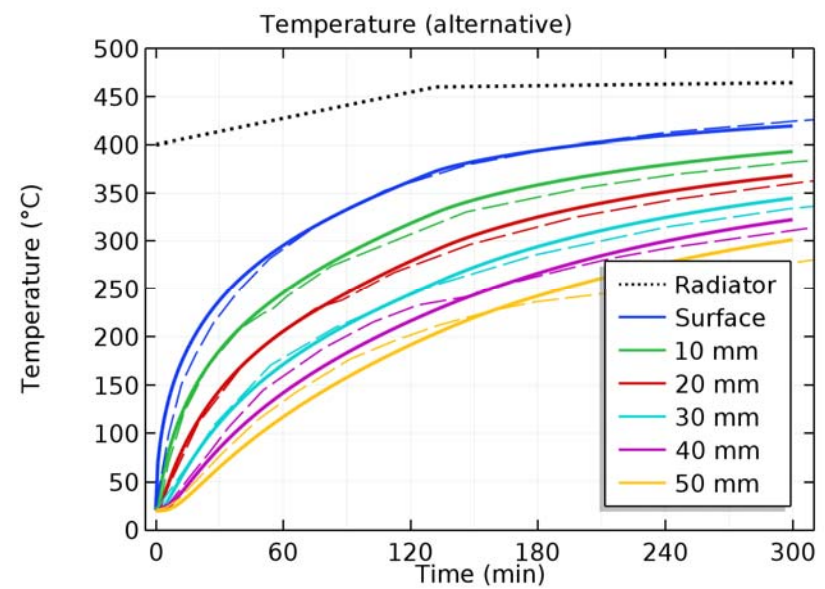
Kalifa, et al., Spalling and pore pressure in HPC at high temperatures, *Cement and concrete research*, **30**, 1915-1927 (2000).

Temperature

Classic



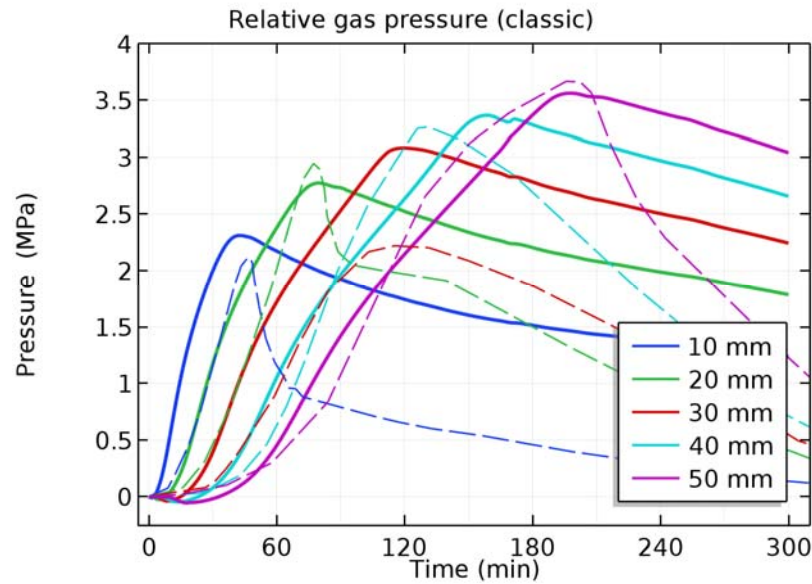
Alternative



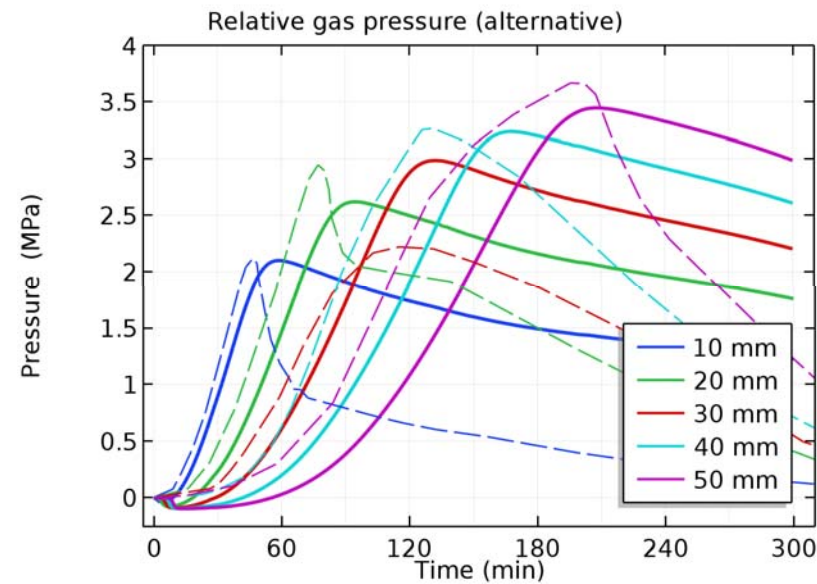
- Identical results

Pore pressure

Classic

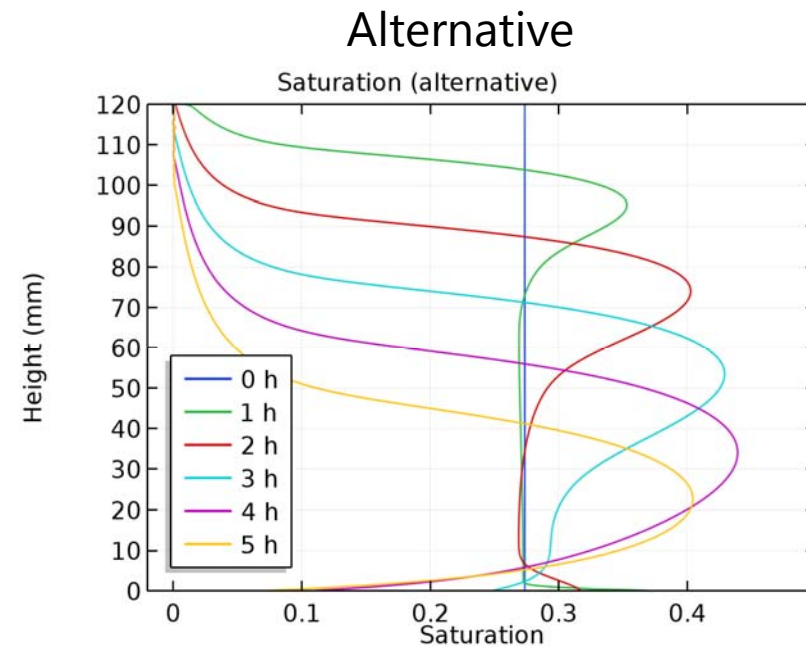
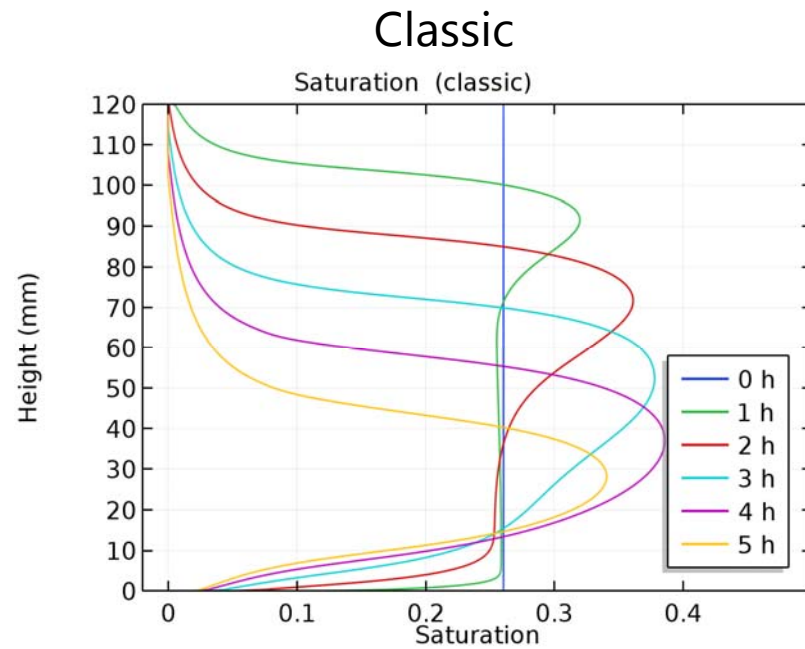


Alternative



- Similar profiles
- Better shape at beginning

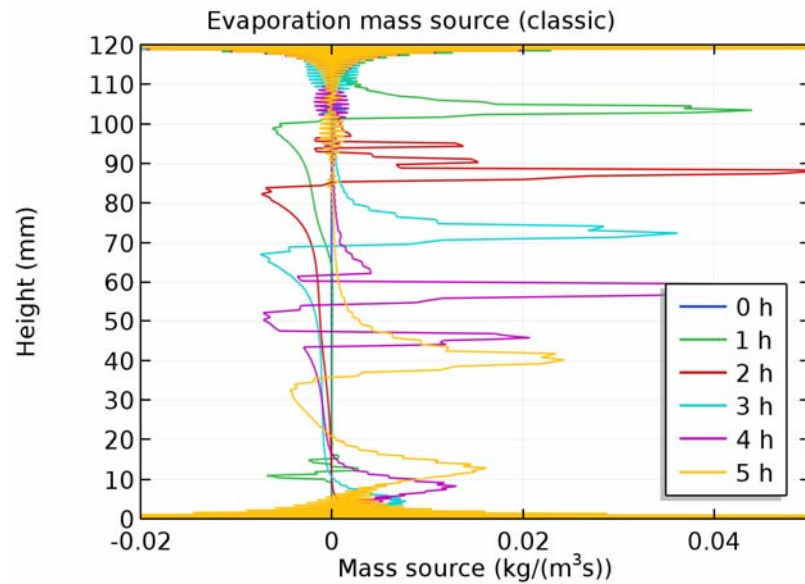
Saturation profile



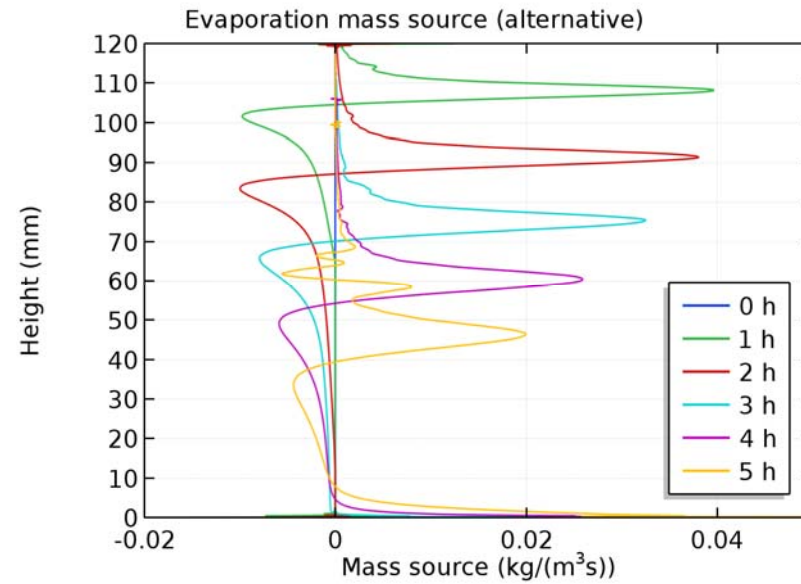
- Very similar
- Different at boundaries

Evaporation mass profile

Classic



Alternative

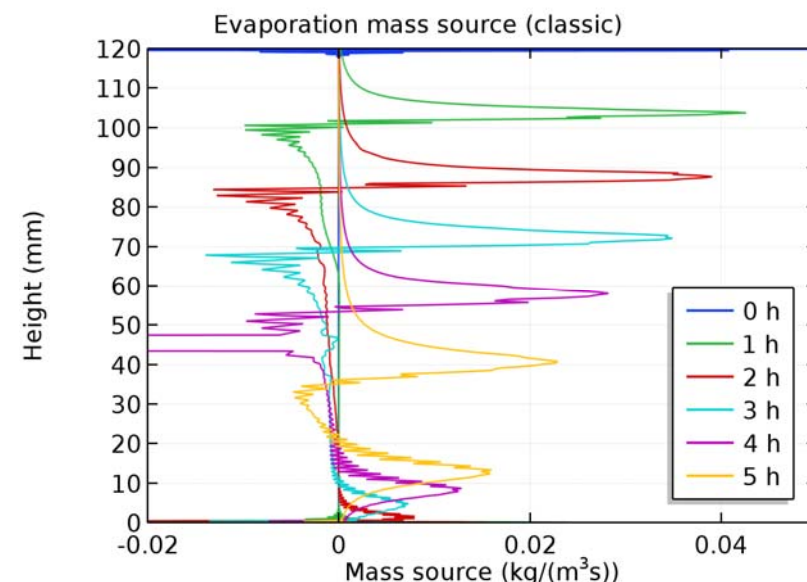
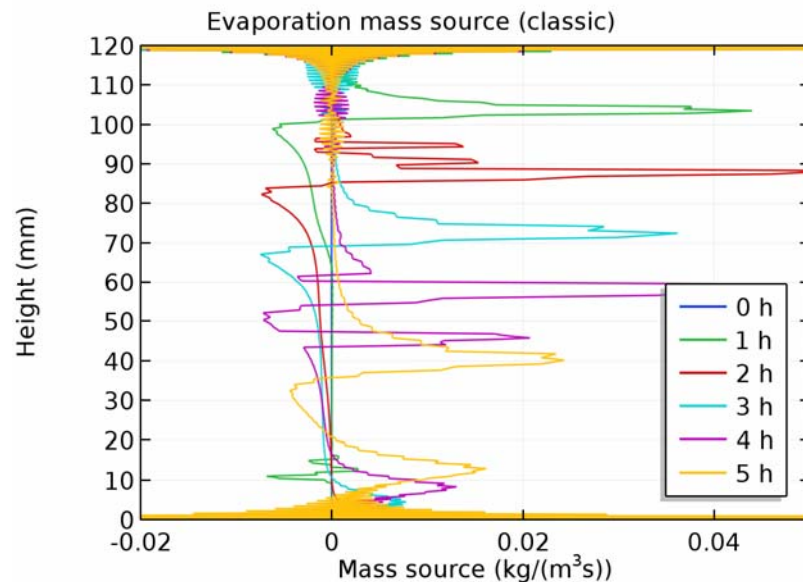


- Globally similar
- Classic more noisy

Evaporation mass profile, classic formulation

Postprocessing with vapor conservation

Postprocessing with liquid conservation



- Simulation and postprocessing with evaporation mass from vapor or liquid conservation equation
- Results depend mainly on postprocessing not on simulation

Discussion

Classic

- Similar pressure and saturation
- Noisy evaporation mass
- Difficult interpretation for $T > T_{cr}$
- Faster execution time (70 s)
- Numerical tweaks necessary

Alternative

- Similar pressure and saturation
- Smooth evaporations mass
- Correct physics for $T > T_{cr}$
- Slower execution time (130 s)
- Additional primary variable and regularization

Conclusions

- Alternative formulation to avoid nonphysical details of classical model, in particular, avoid capillary pressure as primary variable, since not physical when $S=0$ or $T > T_{cr}$
- Use non-equilibrium formulation: evaporation proportional to pressure difference (equilibrium pressure – actual pressure)
- Extra effort, but more rational physics
- Similar pressure and saturation, since relevant processes occur below T_{cr}
- Relatively easy to make major model changes and try different formulations with Equation-Based Modeling